AN IMPLICIT HEATING PROGRAMME TO MINIMIZE THE EFFECT OF THE DIFFERENCE BETWEEN THE SAMPLE TEMPERATURE AND THE PROGRAMMED TEMPERATURE

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An implicit heating programme is suggested for minimization of the effect of the difference between the sample temperature and the programmed temperature in a thermoanalytical set-up.

In a previous paper [1], a heating programme was reported which minimizes the difference between the programmed temperature and the sample temperature during a physical or chemical process followed in a thermoanalytical set-up. The programme was obtained through minimization of the integral

$$I = \int_{0}^{\infty} (T_p - T_s) \,\mathrm{d}t \tag{1}$$

where T_p and T_s are the programmed and sample temperatures, respectively, and t is time. To ensure a minimum of the integral (1), a supplementary imposed isoperimetric condition was used.

In the following, we examine the possibility of minimizing integral (1) without the above condition, and finally suggest another minimization criterion.

John Wiley & Sons, Limited, Chichester Akadémiai Kiadó, Budapest Considerations concerning the minimization of the integral

$$J = -I$$

Instead of I, the integral J, defined by

$$J = \int_{0}^{\infty} (T_s - T_p) \,\mathrm{d}t \tag{2}$$

will be considered for minimization. In order to see whether the minimization is possible or not, the following approximations have to be taken into account:

1. the heat capacity of the sample C_s is constant (it does not change during the transformation);

2. the total heat of reaction ΔH does not change with the temperature T and the conversion degree α ($\Delta H = \text{const.}$).

In isothermal kinetics, the physical or chemical change undergone by a sample is described by the differential equation:

$$\frac{d\alpha_s}{dt} = Af(\alpha_s) e^{-\frac{E}{RT}} \qquad (T = \text{const.})$$

$$(A = \text{const}; E = \text{const.})$$
(3)

which, accepted as a P-PIDKE and with the application of the classical nonisothermal change (CNC) [2-4], turns into a nonisothermal differential kinetic equation.

The programmed and sample temperatures, respectively are given by the relationships [4]:

$$T_p = h(t) \tag{4}$$

$$T_s = h(t) - \frac{\Delta H}{C_s} \alpha_s + T_1 \tag{5}$$

where T_1 is the term corresponding to the heat transfer between the sample and the heating block, and h(t) is the heating programme which has to be obtained. No matter what its explicit form, the programme has to fulfil the obvious initial condition:

$$h(t = 0) = T_0 (6)$$

where T_0 is the initial temperature of the sample.

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The following differential equation describes the evolution of T_1 in time:

$$\frac{\mathrm{d}T_1}{\mathrm{d}t} = -\frac{K}{C_s} \left(-\frac{\Delta H}{C_s} \alpha_s + T_1 \right) \tag{7}$$

where K = const. is the heat transfer coefficient between the sample and the heating block.

We shall accept that the whole sample at a given moment is characterized by the temperature given by (4). All the further calculations will be performed by considering that the process which occurs in the sample is exothermic, $\Delta H < 0$, and thus $T_s \ge T_p$. The endothermic case could be treated in the same way merely by changing the sign.

Equation (4) for the particular condition K=0, when, according to (6):

$$T_1 = 0$$
 (8)

turns into:

$$T_{s} = h(t) = \frac{\Delta H}{C_{s}} \alpha_{s}$$
⁽⁹⁾

Through the CNC [3, 4], Eq. (2) takes the form:

$$\frac{\mathrm{d}\alpha_{s}}{\mathrm{d}t} = Af(\alpha_{s})e^{-\frac{E}{RT_{s}}} \tag{10}$$

For the considered case, taking condition (2) into account, it turns out that:

$$J_1 = \int_0^\infty -\frac{\Delta H}{C_s} \alpha_s \,\mathrm{d}t \tag{11}$$

It is seen from Fig. 1, that the value of J_1 is ∞ , and thus its minimization is meaningless.

Actually, it would be more correct to minimize the integral J_2 given by

$$J_{z} = \int_{0}^{t_{z}} -\frac{\Delta H}{C_{s}} \alpha_{s} \,\mathrm{d}t \tag{12}$$

where t_2 is the time corresponding to almost the completion of the process which occurs in the sample (for instance, t_2 should be taken as corresponding to $\alpha_s = 0.99$). Since t_2 depends on the heating programme, relationship (12) cannot be recommended for minimization.

If T_s is given by relationship (5), one has to minimize the integral J_3 given by:

$$J_3 = \int_0^\infty \left(-\frac{\Delta H}{C_2} \alpha_s + T_1 \right) dt$$
 (13)

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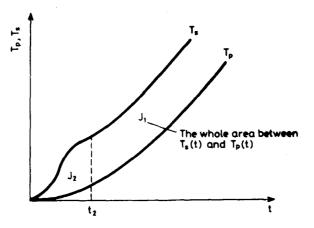


Fig. 1 Temperatures T_s and T_p vs. time (T_s given by Eq. (9))

Introducing the notation:

$$-\frac{\Delta H}{C_s}\alpha_s + T_1 = \Delta T(t) \tag{14}$$

the integral J_3 can be written briefly as:

$$J_3 = \int_0^\infty \Delta T(t) \,\mathrm{d}t \tag{15}$$

From (14), through differentiation, one obtains:

$$-\frac{H}{C_s}\mathrm{d}\alpha_s + \mathrm{d}T_1 = \mathrm{d}\Delta T(t) \tag{16}$$

where, taking condition (6) into account:

$$-\frac{\Delta H}{C_s} d\alpha_s - \frac{K}{C_s} \Delta T(t) dt = d\Delta T(t)$$
(17)

From (17), through integration for $\alpha_s \in [0, 1]$ and $t \in [0, \infty]$, it turns out that:

$$-\frac{\Delta H}{C_s} = \int_0^\infty \left(-\frac{K}{C_s}\right) \Delta T(t) \,\mathrm{d}t = 0 \tag{18}$$

or

$$\int_{0}^{\infty} \Delta T(t) \, \mathrm{d}t = -\frac{\Delta H}{K} = J_3 \tag{19}$$

This result is shown graphically in Fig. 2.

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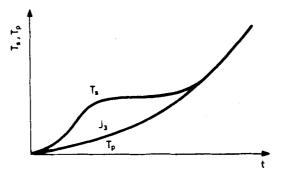


Fig. 2 Temperatures T_s and T_p vs. time (T_s given by Eq. (5))

Thus, no matter what the heating programme, the value of the integral J_3 is constant, i.e. the total area under the curve T(t) is invariant to the heating programme if C_s , ΔH and K are constant.

Since these results show that criterion (1) fails under the considered conditions, another minimization criterion must be suggested.

Let us suppose that in a thermoanalytical set-up the reference crucible contains a compound which undergoes a reaction with the same kinetic parameters as in the sample, but without any thermal effect.

This hypothetical compound will be denoted by s^* .

The kinetics of the processes which occur in the sample and in the reference compound, respectively, are described by the equations:

$$\frac{\mathrm{d}\alpha_s}{\mathrm{d}t} = Af(\alpha_s)e^{-\frac{E}{R(h(t) - \Delta H/C_s\alpha_s + T_1)}} \tag{20}$$

$$\frac{\mathrm{d}\alpha_{s*}}{\mathrm{d}t} = Af(\alpha_{s*})e^{-\frac{E}{Rh(t)}}$$
(21)

In this case, another criterion of minimization can be suggested by looking for the minimum of the integral:

$$J_4 = \int_0^\infty \left(\alpha_s - \alpha_{s^*} \right) \mathrm{d}t \tag{22}$$

i.e. one has to minimize the area between the curves $\alpha_s(t)$ and $\alpha_{s*}(t)$ (Fig. 3).

The advantage of such a criterion results from the following theorem, which will be stated without demonstration.

If α_1 and α_2 are the conversion degree at a given moment, corresponding to two heating programmes $T_1 = \theta(t)$ and $T_2 = \theta(t) + \theta_1(t)$ with $\theta_1(t) > 0$, then the curves $\alpha_1(t)$ and $\alpha_2(t)$ satisfy the following two conditions:

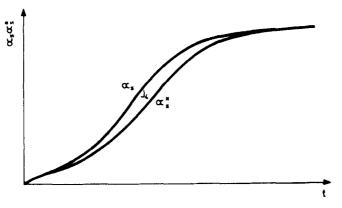


Fig. 3 Conversions α_s and α_{s*} vs. time

1. Except for t=0 and $t=\infty$, the curves $\alpha_1(t)$ and $\alpha_2(t)$ do not intersect.

2. The area limited by the curves $\alpha_1(t)$ and $\alpha_2(t)$ is a finite quantity which depends on the heating programme.

It is easy to see that $\left(-\frac{\Delta H}{C_s}\alpha_s + T_1\right) > 0$, i.e. the heating programmes (5) and (9) satisfy the above-mentioned conditions.

Conclusions

The minimization of the effect of the temperature difference between the sample and the reference requires a heating programme, h(t), which can be found by considering the equations:

$$\frac{d\alpha_{s}}{dt} = Af(\alpha_{s})e^{-\frac{E}{R(h(t) - \Delta H/C_{s}\alpha_{s} + T_{1})}}$$

$$\frac{d\alpha_{s*}}{dt} = Af(\alpha_{s*})e^{-\frac{E}{Rh(t)}}$$

$$\frac{dT_{1}}{dt} = -\frac{K}{C_{s}}\left(-\frac{\Delta H}{C_{s}}\alpha_{s} + T_{1}\right)$$

$$J_{4} = \int_{0}^{\infty} (\alpha_{s} - \alpha_{s*}) dt - \text{minimum}$$
(23)

With regard to the mathematical difficulties, we leave the finding of the explicit form of h(t) from conditions (23) as an open question.

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References

- 1 E. Segal and M. Vlad, Thermochim. Acta, 16 (1976) 115.
- 2 E. Urbanovici and E. Segal, Thermochim. Acta, 111 (1987) 335.
- 3 E. Urbanovici and E. Segal, Thermochim. Acta, 118 (1987) 65.
- 4 E. Urbanovici and E. Segal, Thermochim. Acta, in press.

Zusammenfassung — Es wird ein implizites Aufheizprogramm beschrieben, das den Einfluss des Unterschiedes zwischen Probentemperatur und programmierter Temperatur für die Probe minimalisiert.

Резюме — Предложена скрытая программа нагрева с целью свести до минимума влияние различия между температурой образца и запрограммированной температурой в термоаналитической установке.